Guidance on safety integrity level determination for safety instrumented systems in support of IEC 61511

energy institute

GUIDANCE ON SAFETY INTEGRITY LEVEL DETERMINATION FOR SAFETY INSTRUMENTED SYSTEMS IN SUPPORT OF IEC 61511

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1 INTRODUCTION, SCOPE AND APPLICATION

1.1 INTRODUCTION

Most process plants are controlled by complex process control systems; there is increasing dependence on safety instrumented systems (SISs) to carry out safety instrumented functions (SIFs).

After applying inherently safer design (ISD) principles to the fundamental process plant design to eliminate hazards as the first priority, residual process plant hazards should be properly controlled and have effective risk reduction measures (RRMs) in place to achieve target risk levels. Equipment on the process plant and the process control system may provide some risk reduction, but these do not usually provide sufficient control for all the identified hazardous events. Consequently, to achieve target risk levels, and as part of a balanced approach to risk reduction, additional RRMs may be necessary. Such RRMs could include SISs to carry out SIFs. These are protection layers (PLs) that are intended to detect abnormal conditions on the process plant and prevent the hazardous event (PL(prevention)), or to mitigate the consequences of the hazardous event (PL(mitigation)). SISs comprise electrical, electronic or programmable electronic systems.

To achieve target risk levels, the approach should involve (in order of priority):

- Applying ISD principles (also in order of priority):
  - elimination of hazards, and
  - control and minimisation of risk at source using physical engineering controls (e.g. by increasing separation distances).
- Providing PLs (prevention) that reduce the specific hazardous event frequency (HEF). These may include systems and functions that are intended to detect abnormal conditions on the process plant and prevent the hazardous event.
- Providing PLs (mitigation) that mitigate the consequence of the specific hazardous event. These may include systems and functions that are intended to mitigate the consequences of the hazardous event.

For a specific hazardous event, the objective of SIL determination is to:

- Determine whether it is necessary to employ a SIS to carry out a specific SIF, where there is a shortfall in the risk reduction already achieved by RRMs to meet a target risk.
- Determine the SIL of the SIF where it has been determined that there is a shortfall in the risk reduction needed to meet the target risk.

An example of a hazardous event is 'Rupture of pressure vessel and release of flammable gas at high pressure leading to an extensive gas cloud.'

Whilst the guidance provided in this technical publication relates to the required performance of the SIFs to be implemented by PLs to prevent hazardous events or to mitigate the consequences of hazardous events, selecting SIFs and determining their performance requirements should be part of a balanced approach to risk reduction.

1.2 INDUSTRY CONTEXT

There is increasing dependence on SISs to carry out SIFs to achieve target risk levels (e.g. tolerable). Recent process industry incidents such as those occurring at petroleum refineries and bulk storage facilities have focused attention on several issues related to the design and maintenance of functional safety of SISs if the target risk levels are to be achieved.

1.3 SCOPE

This technical publication supports practical application of the following clauses of IEC 61511-1:

- clause 8 Process H&RA, and
- clause 9 Allocation of safety functions to protection layers.

It does so by providing guidance on:

- SIL determination of SIFs associated with SISs within the scope of IEC 61511.
- Identifying the SIFs to be carried out by one or more SISs.
- Illustrating several SIL determination methods available for ensuring that an appropriate SIL is selected for each SIF.
- The team-based workshop methodology.

Guidance is provided on some key principles and requirements for effective functional safety management (FSM), including:

- Setting a target risk comprising target harmful event frequencies for the specified consequences (e.g. safety and environment).
- Justifying the basis on which the target harmful event frequencies for specified consequences are set.
- Having a rational basis for claims made for the risk levels that are achieved.
- Ensuring that the assumptions relating to the risk reduction parameters that impact on the amount of risk reduction that is being claimed for a particular PL are based on robust evidence and are managed throughout the life of the process plant.

This technical publication focuses on quantitative and semi quantitative SIL determination techniques. It is, however, acknowledged that a qualitative approach to SIL determination may be appropriate, such as where there is available authoritative guidance on SIL determination that provides a rational basis for its target risk criteria. For more severe harmful event consequences, a quantitative and semi quantitative approach to SIL determination should be used.

Worked examples are provided to illustrate key points.

Excluded from the scope is guidance on other key steps of the SIS safety life cycle, from SIS design and engineering through installation and commissioning to decommissioning; for guidance, see EI *Guidance on achievement, operation and maintenance of functional safety employing safety instrumented systems in support of IEC 61511*.

1.4 MEETING SAFETY AND ENVIRONMENTAL LEGAL REQUIREMENTS

IEC 61511 provides a benchmark of good practice in the achievement of functional safety for the process industry; as an international standard, it has a level of acceptance by safety and environmental regulators, which should assist duty holders in demonstrating compliance with pertinent legislation and regulations. The intent is that this technical publication further facilitates demonstration of compliance with pertinent legislation and regulations, as well as for risk types that are not subject to legislation and regulations (e.g. asset risk – see 1.5).

1.5 RISK TYPES AND CRITERIA

This technical publication covers the selection of a target risk (i.e. a target harmful event frequency for a specified consequence). Annex D provides illustrative target harmful event frequencies that should assist in the determination of the following risk types:

- Individual risk: safety risk for a hypothetical person (an individual worker) for a specified scenario, where the consequence is a fatality or injuries.
- Group risk: safety risk for a specified scenario, where the consequence is multiple fatalities or injuries.
- Environmental risk: risk to receptors from all hazardous events at the whole establishment, where the consequence is harm, whose impact is considered by its severity and duration.
- Asset risk: risk to businesses for a specified scenario, where the consequence is disruption to operation or costs.

Although Annex D does not provide illustrative target harmful event frequencies in relation to societal risk (i.e. societal concerns due to the occurrence of multiple fatalities in a single event), this technical publication is still relevant when the target harmful event frequency has been established based on societal risk criteria. See HSE *R2P2*.

1.6 APPLICATION

As this technical publication supports practical application of some aspects of IEC 61511-1, then the current edition of IEC 61511-1 is a normative reference, i.e. it is indispensable when applying the guidance herein.

The intended applications of this technical publication are:

- The process industry sectors (e.g. nuclear processing, offshore and onshore oil and gas sectors, and the chemical manufacturing industry).
- SIFs operating in any mode of operation (i.e. low demand, high demand or continuous mode).
- New process plant design, but also legacy systems where modifications are being considered or undertaken.